Life cycle inventory of samarium-cobalt permanent magnets, compared to neodymium-iron-boron as used in electric vehicles

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Electric vehicles are sometimes marketed unambiguously as low-carbon technologies; however, they often contain less ‘clean’ ingredients, such as rare earth elements. High-performance

permanent magnets in electric vehicles often use neodymium. Alternatively, samarium-cobalt magnets can be used. In this paper, life cycle assessment is used to compare the primary production routes of both neodymium-iron-boron and samarium-cobalt magnets in terms of environmental impact. For primary production of samarium-cobalt magnets, this is the first life cycle assessment published to date. In addition, a life cycle assessment of neodymium-iron-boron is updated and expanded with recent literature and some primary industry data.

The conclusion is that the production of samarium-cobalt is not preferable in terms of environmental impact from a cradle-to-gate perspective. A sensitivity analysis and uncertainty analysis show that while there are uncertain parameters in both studies, the uncertainty range tends to be slightly higher for samarium-cobalt.

1. Introduction.

Paradoxically, the materials used in the low carbon technologies of the future are often sourced in an environmentally-damaging and carbon-intense way; permanent magnet production is not different. The advancement of permanent magnets (PM) is driven by the miniaturization of magnetic material coupled with increased property performance. The environmental damage associated with the production of these magnets is of increasing concern both to policy makers and industry. As such, the choice of magnetic alloy should be further considered in terms of product design for PMs in electric motors.

Prior to the 1980s, the best temperature-resistant and energy-dense product magnets available were samarium-cobalt (SmCo) based and could be found in a majority of PM applications (Strnat, Hoffer, Olson, Ostertag, & Becker, 1967). However, the Japanese company Sumitomo and the American company General Motors wanted to develop a way to maintain magnet performance at

a lower cost (Krishnamurthy & Gupta, 2005). Thus the neodymium-iron-boron (NdFeB) magnet was developed (Herbst, Croat, Pinkerton, & Yelon, 1984; Sagawa, Fujimura, Yamamoto, & Matsuura, 1985). The rapid transition from SmCo to NdFeB was also partly due to problems with the supply of cobalt. Civil unrest (in 1978) in the Democratic Republic of Congo, formerly Zaire, threatened about half the world's supply of refined cobalt metal. At that time, NdFeB was found to be an appropriate substitute for SmCo as it was both cheaper, less subject to price volatility, and supply was not deemed at risk. Since then, NdFeB magnets have been the standard choice of PM used in most electronic applications such as hard disk drives, cell phones, and electric vehicle motor/generators.

Nevertheless, SmCo does retain some advantages over NdFeB. These include better corrosion resistance and greater magnetic output at temperatures above ca. 150°C. The elevated temperatures of a vehicle drive train require magnets with superior coercivity. Adding dysprosium or terbium could improve NdFeB magnets' Curie temperature and higher temperature performance (Chen et al., 2015). But both dysprosium and terbium are heavy rare earth elements (HREE) with relatively low reserves bases and both are significantly more expensive than neodymium. In some cases, this makes the use of SmCo magnets more cost-effective (Magenti Ljubljana, 2013). Despite these advantageous properties, the market share of SmCo for PMs is around 2% (Binnemans et al., 2013). It should be noted that changing the chemical compositions of the magnets will affect the stability and the magnetic strength could be jeopardized. Note that using different magnet types may also affect the design of the motors, thus indirectly affect the environmental footprints. This aspect is not considered in the current study.

While several life cycle assessment (LCA) studies have been performed for NdFeB magnets, (Marx, Schreiber, Zapp, & Walachowicz, 2018; Sprecher et al., 2014) and other oxide forms of rare earth elements (REEs) (Navarro & Zhao, 2014; Schreiber et al., 2016; Tharumarajah & Koltun, 2011; Vahidi, Navarro, & Zhao, 2016), we are not aware of any previous SmCo magnet LCA studies. In this work we answer the question: will the substitution of NdFeB-based PMs by SmCo-based PMs reduce environmental impact?

2. Methodology

LCA methodology was used to compare the environmental impact of producing 2.04 kg of SmCo magnet with 1 kg of NdFeB magnet, in accordance with Guinée et al. (2002). The LCI was constructed using the software package GaBi (version 8.5). To enable comparison with the previous study by Sprecher et al. (2014) the CML2001 – 2013 impact assessment method was used. Section 2.1 contains the goal and scope of this study. Section 2.2 describes the life cycle inventories (LCIs) for the production of NdFeB and SmCo. The full LCIs for both processes are provided in the Supporting Information.

2.1 Goal and Scope

The system boundaries of the present study include the entire production chain of both neodymium-iron-boron and samarium-cobalt PMs, from mining to the production of the magnet. We do not consider the use and end-of-life (EoL) phases. See Scheme 1 for a schematic representation.

As a functional unit, we use the energy density and functionality of 1.0 kg of NdFeB. This is matched by 2.04 kg of SmCo, based on the magnetic energy density per unit volume,

85 referred to as the maximum energy product or $(BH)_{\max}$. See Table 1 for conversion
86 parameters.

87 **Table 1.** Conversion of magnets maximum energy product into energy per kg

	Magnetic energy density kJ/m ³	Density kg/m ³	Magnetic energy per unit mass kJ/kg	Relative magnetic energy per unit mass -
NdFeB	450	7625	0.059	1 (reference)
SmCo	240	8300	0.029	2.04

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Scheme 1. Processing flowsheet differences between SmCo (left) and NdFeB (right)

2.2 Life cycle inventory of NdFeB and SmCo Production

Although the production processes of NdFeB and SmCo differ significantly, parts of the REE production and final stages of magnet production overlap, as seen in Scheme 1. For REE production, the processes differ after solvent extraction (SX). Magnet production differs until it converges at jet milling. We first discuss the life cycle inventory (LCI) of NdFeB in section 2.2.1, followed by a description of the LCI of SmCo in section 2.2.2.

2.2.1 NdFeB Life Cycle Inventory

The NdFeB LCI is based on Sprecher et al. (2014), updated to include the latest data available. First, all background processes were updated to Ecoinvent version 3.3 (Wernet et al., 2016); second, the proxy used for ‘organic chemicals’ was updated with recent data on solvents in Vahidi and Zhao (2016) and Vahidi and Zhao (2017). Third, several values in the beneficiation and SX processes were updated according to Lee and Wen (2017). Finally, rare earth oxide (REO) values were updated to reflect the past 10 year average prices. The latter led to a shift in allocation in the SX process, because REO prices decreased from Sprecher’s original figures (from 85 USD per kg of Nd_2O_3 to 45 USD per kg). Finally, we note that for electroplating of NdFeB, it was not possible to obtain values for wastewater. This could yield significant effects since 1 m^3 of wastewater treatment for black chrome nickel plating results in a Global Warming Potential (GWP) impact of 0.2 kg of CO_2 per kg of magnet.

A complete overview of the final data used in this study for each process can be found in the Supporting Information – NdFeB LCI, where changes from Sprecher et al. (2014) are highlighted in red.

2.2.2 SmCo Life Cycle Inventory

Due to the lack of LCI data within the rare earth industry (Bailey et al, 2020), our SmCo LCI data are based on a mixture of literature sources, industry data, interviews with experts, and Ecoinvent background data (Table 2). An overview of the SmCo production process and modeling choices are described in the following sub-sections. A detailed discussion of the assumptions can be found in the Supporting Information. The full LCI data can be found in the Supporting Information – SmCo LCI.

Table 2. LCI (foreground and background) sources for SmCo LCA

<i>Production Stage</i>	<i>References</i>
Mining	(Sprecher et al., 2014), Ecoinvent, Thinkstep, (IEA, 2011) (Norgate & Haque, 2010),(The Cobalt Development Institute, 2016)
Beneficiation	(Peiró & Méndez, 2013), Ecoinvent, Thinkstep, (Sprecher et al., 2014),(Lee & Wen, 2017), (IEA, 2011)
Acid Roasting	(Sprecher et al., 2014), Ecoinvent, own calculations
Leaching	(Sprecher et al., 2014), Ecoinvent, own calculations
Solvent Extraction	Ecoinvent, (Lee & Wen, 2017), Calculations, (Sprecher et al., 2014)
Lanthanum Reduction	(Lee & Wen, 2017), (Ministry of Environmental Protection, 2009), Thinkstep, (Krishnamurthy & Gupta, 2005)
Book Molding	Ecoinvent, Industrial source, (The Cobalt Development Institute, 2016)
Coarse Milling	Ecoinvent, Industrial source

Jet Milling	(Sprecher et al., 2014), Industrial source, Ecoinvent
Aligning and Pressing	Industrial source
Sintering	Industrial source, (Sprecher et al., 2014), Ecoinvent
Grinding and Slicing	Ecoinvent, Industrial source
Electroplating	Ecoinvent, (Moign, Vardelle, Legoux, & Themelis, 2009), (Sprecher et al., 2014), Industrial source

Cobalt Mining and Production Route

Cobalt production is based on the LCI dataset provided by the Cobalt Development Institute (CDI), which is based on primary data coming from eight cobalt producers, representing 30% of total global production. As such it is currently the most comprehensively available LCI data on cobalt (The Cobalt Development Institute, 2016). The dataset covers the production of cobalt (metal and powder) obtained as a co-product from mining/production of both nickel and copper, and applies a combination of mass allocation and economic allocation, since cobalt attracts a higher price than its main co-products (The Cobalt Development Institute, 2016) (Santero & Hendry, 2016).

Samarium Mining and Beneficiation

The mining and beneficiation of samarium follows a similar route to that of neodymium as described in Sprecher et al. (2014), with values being adjusted to account for the main product being samarium rather than neodymium (i.e. the total ore required to produce the functional unit).

Many types of ore contain samarium, with bastnaesite being the most common ore from which samarium is produced (Li & Yang, 2014). Although bastnaesite is not the richest in samarium, its rich overall REEs content and simple composition make it the most convenient to process for the production of all REEs, in particular of the light ones, such as samarium (Shi, 2009). Sprecher et al. (2014) also considered bastnaesite as the source of neodymium and samarium. The largest site of bastnaesite is Bayan Obo in Inner Mongolia but not all samarium is produced from bastnaesite. Although environmental and energy data for this mine is largely kept confidential due to

commercial sensitivity, recent studies provide information on Chinese specific emissions from Chinese standards but it is not necessarily specific to any facility (Chinese Ministry of Environmental Protection, 2011; Lee & Wen, 2017). The mining process in Bayan Obo is both physically and chemically similar to iron ore mining. Environmental inflows and outflows of the process are therefore assumed to be the same, except for the difference in ore concentration which has been calculated (Li & Yang, 2014). The model for the beneficiation process includes the combination of chemicals and energy used for removal from REEs concentrate from a tailings stream containing predominantly Fe₂O₃. Ores are initially crushed to the desired particle size. A series of weak and then strong magnetic separation removes iron from the ore to be processed separately. The last step is froth flotation, where fatty acid collectors are added which adhere to the bastnaesite. This causes them to float to the surface of the solution where they can be captured.

Acid Roasting and Leaching

The acid roasting process is based on Sprecher et al. (2014), See Supporting Information – SmCo LCI for more detailed information.

At the Bayan Obo mining site, the mineral concentrate from beneficiation is roasted with sulfuric acid and then leached. Sulfuric acid is a common reactant to dissolve mixed concentrates containing carbonatite minerals. This high-temperature acid-roasting process is relatively simple but generates potentially hazardous exhaust gases such as hydrogen fluoride (HF). These hazardous products can be removed by scrubbing before releasing the gas into the environment. However, this is not known as a common practice in China. The main reaction is given in equation (1):

168 The radioactive elements present in the ore react with the sulfuric acid, as given in equations 2 and
169 3:

172 The content of ThO_2 and U_3O_8 in the ore are, respectively, <0.3 wt.% and <0.1 wt.%, and are
173 calculated based on the proportion of a samarium content equal to 0.8 wt.% (Jordens, Ping
174 Cheng, & Waters, 2013) (IEA, 2011). In equation 3, the consumption of O_2 from air is negligible
175 in terms of quantity. The total consumption of H_2SO_4 is not stoichiometric. In fact, an
176 acid/mineral mass ratio between 1:1 and 2:1 is used to face the consumption of acid that derives
177 from high content of carbonates and iron in the gangue. The ratio varies between 1:1 and 2:1. To
178 be conservative, the present study uses an average ratio of 1.7. The results are listed in Table 3.
179

Table 3. Mass balance of the acid roasting, with basis of 1 kg of $\text{REE}_2(\text{SO}_4)_3$ in output. Detailed calculations found in Calculations supporting document.

<i>Compound</i>	<i>Mass (kg)</i>
$\text{REE}(\text{CO}_3)\text{F}$	0.53
$\text{REE}(\text{PO})_4$	0.30
H_2SO_4	0.37
H_2O	0.07
ThO_2	0.01
$\text{Th}(\text{SO}_4)_2$	0.15
U_3O_8	0.03
UO_2SO_4	0.05
$\text{REE}_2(\text{SO}_4)_3$	1.00

182

183 After that, the $\text{REE}_2(\text{SO}_4)_3$ is converted into a REECl_3 in a leaching step. This is carried out
184 according to the reaction:

186 Table 4 lists the results assuming a leaching efficiency of 92%, as in Sprecher et al. (2014).

187

Table 4. Mass balance of the conversion of $\text{REE}_2(\text{SO}_4)_3$ into chlorides with assumed output of 1.00 kg of REECl_3 . Detailed calculations found in Calculations supporting document.

Compound	Mass (kg)
$\text{REE}_2(\text{SO}_4)_3$	1.20
HCl	0.82
Na_2CO_3	1.19
H_2CO_3	0.38
Na_2SO_4	2.03
REECl_3	1.00

An excess of acid is used to have a good liquid to solid ratio, but the unreacted acid, recovered from the residue, is recycled and does not count in the emissions to the environment.

Solvent Extraction

Separating individual REEs from concentrates is a very difficult process due to their similar chemical properties (Morais & Ciminelli, 2004). Solvent extraction (SX) is the most widely used separation technology to separate light REEs from heavy REEs at the industrial scale (El-Nadi, 2017). The modeled process consumes 152 kg of REECl_3 concentrate to produce 1 kg of 98.99% Sm_2O_3 . As a co-product, 85 kg of other REOs are produced.

Economic allocation was applied for both Nd_2O_3 and Sm_2O_3 and the rest of REOs. Due to the volatility of REEs prices, we employed the price averaging approach recommended for mining and metals (Santero & Hendry, 2016).

Industrial SX is carried out in groups of mixer-settlers, called batteries. The process is ineffective if only performed once, as the chemical properties of all the REE are very similar, making

separation a challenge. Only with repeated SX steps are the REEs successfully separated from each other. Due to confidentiality reasons, it is not known how many steps exactly are needed to separate SmCl_3 from the other REOs. The estimation used in this study is based on a calculation of what is *chemically* needed for a separation of SmCl_3 from the other REOs to occur. Generally, most REE extraction operations do not separate SmCl_3 , since it is a low value REE (Supporting Information, Table S-3).

Industrial REE SX processes work with modifiers, extractants, and solvents. The SX process modeled uses organic molecules (represented as P204, or $\text{C}_{16}\text{H}_{35}\text{O}_4\text{P}$ in this model), often diluted in organic solvents (represented as kerosene in this model). These solutions are able to form stable complexes with the REEs and subsequently are able to be extracted from the feeding solution with a precipitating agent (oxalic acid in this case). Typically, calcination, heating the oxalates and obtaining a calcine, follows the process of SX. The purpose of calcination is to obtain an oxide through thermal decomposition of REE oxalates to give REE oxides and CO_2 . The SX, precipitation, and calcination were all combined in one step to produce 1 kg of Sm_2O_3 . This method of combining of steps was also carried out in (Sprecher et al, 2014).

Reduction

After the SX stage, the production of SmCo alloy differs significantly from that of NdFeB alloy. Rather than electrolysis (as for neodymium oxide), the Sm_2O_3 is reduced using metallic lanthanum. According to one of the only European companies producing REE alloys, this route is the most popular route for producing samarium metal. The relatively low vapor pressure of samarium at the working conditions causes the samarium to evaporate from the hot mixture of oxides, the samarium vapor leaves the system and the reaction equilibrium is shifted to the right according to the Le Chatelier principle. The reaction is as follows:

228 The lanthanum metal is generally heated with the Sm_2O_3 powder at 1330 °C for several hours
229 (Krishnamurthy & Gupta, 2005). The electricity requirement and other LCI parameters were taken
230 from industry surveys in Lee and Wen (2017).

231 [Book molding](#)

232 The casting process starts with broken pieces of book mould of SmCo. The energy consumption
233 was given by an industrial source which uses this process to cast SmCo alloys, reported at 3.6 MJ
234 per kg of material.

235 [Coarse milling and Jet milling](#)

236 According to an industrial source, the SmCo production process uses coarse milling, but not jet
237 milling since the latter poses a safety risk in transporting very fine particles of SmCo, which are
238 pyrophoric. Coarse milling uses both argon and nitrogen gas. The energy consumption for coarse
239 milling is about 18 MJ per kg of product. For jet milling, the NdFeB data was extrapolated using
240 the temperature profile of SmCo to appropriate the energy consumption for jet milling of SmCo_5 .
241 Yield losses on coarse milling are low, typically less than half of one percent. In this work, loss
242 was assumed as 0.5% as a worst-case scenario.

243 [Aligning, Pressing, Sintering, Grinding and Slicing](#)

244 The sintering and heat treatment of SmCo is done in a similar way to NdFeB, with energy and
245 material consumption differing slightly. LCI data was obtained from industrial magnet makers in
246 eastern Europe. The total energy consumption for the aligning, pressing, sintering, grinding and
247 slicing processes combined is reported at 15.12 MJ per kg. Losses occur at sintering (due to heat
248 treatment) and grinding/slicing, modelled as 5 % and 10% loss respectively.

Electroplating

Unlike NdFeB magnets, SmCo magnets do not necessarily require a protective coating (Electron Energy Corporation, 2017; Katter, Zapf, Blank, Fernengel, & Rodewald, 2001), because of the higher corrosion resistance of SmCo magnets. Nevertheless, customers generally prefer to buy SmCo magnets with a nickel coating as an insurance against wear and tear. In addition, SmCo magnets can be very brittle, the coating reduces risk of chipping.

Electroplating emissions data are based on Moign et al. (2009) which was also used in (Sprecher et al, 2014). SmCo magnets were assumed to be electroplated with Ni-Cu-Ni, as indicated by industrial sources. Although both magnets undergo the same electroplating process, the difference in volume of the reference flow leads to different area of nickel coating. We assumed 0.068 m² of a 15 µm layer for 1 kg of NdFeB magnet, and 0.153 m² for the equivalent SmCo magnet.

2.3 Sensitivity and uncertainty analysis

A robust uncertainty and sensitivity analysis is imperative for a highly uncertain system such as REE magnet production, especially when comparing different LCA results (Heijungs, Huppes, and Guinée (2010); Björklund (2002)) underline that in comparative LCAs, in particular, it is necessary to perform a sensitivity analysis to be able to make a comparison between different LCA results, especially when uncertainty distribution functions are unavailable. There are two reasons why a sensitivity analysis is important: (1) it tells you for which parameter affects the model output most (2) if a parameter is very insensitive, it also almost never contributes to the output uncertainty. In this study, a sensitivity analysis was carried out on 23 parameters and the ones with the highest sensitivity percent change (between 2 and 10%) were evaluated in an uncertainty analysis. All parameters surveyed are listed in the Supporting Information, (Table S-8).

Then the sensitivity ratios (SR) were calculated for both magnet systems. These values are obtained by calculating the variability of the relevant impact category using the formula (6).

$$SR = \frac{\frac{\Delta result}{initial\ result}}{\frac{\Delta parameter}{initial\ parameter}} \quad (6)$$

Since the $\pm 10\%$ variation was used, all SR values higher than 0.2 are assumed to be sensitive. The subsequent uncertainty analysis explores the three most sensitive parameters identified by the sensitivity analysis. Uncertainty ranges were constructed using literature and expert interviews (see Supporting Information, Table S-5, S-6, and S-7). After defining uncertainty intervals around the key parameters, we employed Monte Carlo simulation to produce a statistical estimate of the final result as well as its standard deviation across 1,000 simulation runs.

3. Results

The results of the comparative LCA for the production of SmCo and for the production of NdFeB are reported in Table 5. To reiterate, the functional unit is the magnetic performance of 1.0 kg of NdFeB, which is compared with the equivalent 2.04 kg of SmCo.

Table 5. Impact assessment results from comparative LCA

CML 2001	SmCo	NdFeB (Sprecher et al., 2014)	NdFeB (this study)
Global Warming Potential (kg-CO ₂ equiv)	135.0	25.1	30.2
Acidification Potential (kg- SO ₂ equiv)	2.73	0.39	

			3.37
Eutrophication Potential (kg-Phosphate equiv)	0.21	0.16	0.13
Ozone Depletion (kg-R11 equiv)	1.5×10^{-5}	2.4×10^{-6}	1.08×10^{-6}
Freshwater Ecotoxicity Potential (kg-DCB equiv)	83.8	13.8	92.0
Human Toxicity Potential (kg-DCB equiv)	292	179.8	184
Photochemical Ozone Creation Potential (kg-Ethene equiv)	0.130	0.015	0.139

286 In terms of overall greenhouse gas (GHG) emissions, we find that SmCo causes emissions of 135
287 kg of CO₂ equivalent for every 2.04 kg of SmCo magnet whereas NdFeB causes emissions of 30
288 kg.

289 The human toxicity potential results for NdFeB from 2014 are mostly due to the acid roasting
290 process, our results are mostly due to the electroplating (Figure 1). For SmCo, the prevailing
291 contributors to human toxicity potential is the production of cobalt and the acid roasting process.
292 Within the cobalt production process, the highest contributing phase to the global warming
293 potential is the refining of the cobalt metal. For the freshwater aquatic ecotoxicity indicator, the
294 impacts for NdFeB is dominated by the nickel used in the coating, which contributes to aquatic
295 pollution. The freshwater aquatic ecotoxicity indicator for SmCo is also highly impacted by the
296 nickel coating as well as the heavy metals emissions in cobalt production. For SmCo, the wastes
297 and losses modeled throughout the post-processing stages for SmCo are also important.

298 For both SmCo and NdFeB, the major impacts related to acidification are due to the sulfur dioxide
299 emitted in the production of sulfuric acid for the electroplating. For ozone depletion potential the
300 impacts are related to cobalt production in SmCo and the nickel coating in NdFeB production. For
301 photochemical ozone creation potential the main impacts are from cobalt production and
302 lanthanum reduction. A significant contributor to the eutrophication potential and photochemical
303 ozone creation is the production of sulfuric acid used in the primary extraction processes for cobalt.

304 For NdFeB the photochemical ozone creation potential impacts come mainly from the sulfur
305 dioxide emitted in the production of sulfuric acid for electroplating. For eutrophication potential,
306 the main impact comes from the phosphorous emitted to freshwater in cobalt production for SmCo.
307 For NdFeB the same is true for the nickel production for the electroplating. In Figure 1, the
308 contribution of all phases of the REE magnet production to environmental impacts are displayed.
309 The mining and production of cobalt is the highest environmental impact for SmCo, whereas for
310 NdFeB the largest contributor is electroplating.

311

Figure 1. Results of contribution analysis for production of and SmCo (above) and NdFeB (below)

Sprecher's study showed that 37% of the impacts to the NdFeB magnet were due to the nickel coating (Sprecher et al., 2014). For the entire electroplating process, this updated study shows that this impact is around 65% of the total impacts. If one were to forego the nickel coating for a NdFeB or SmCo and replace it with a thin epoxy resin, the impacts would be reduced. However, the nickel coating is almost always applied due to customer preference. A sensitivity analysis was performed on the surface area of the coating for each magnet to show how greatly the impacts would be affected if the surface layer were reduced or increased. The results of these analyses as well as the others are found in section 3.1.

[3.1 Sensitivity analysis](#)

The top three parameters which have the highest sensitivity percent change for both NdFeB and SmCo are: REE content, base metal content, nickel coating layer thickness . We show the results for GWP, since this was the category with the biggest differences. See Supporting Information, Table S-9 and S-10 for the all sensitivity analysis results for input parameters and impact categories of each system.

Figure 2. Sensitivity ratios for Global Warming Potential (variation 10%).

The highest SR in the sensitivity analysis is related to the highest contribution to the final life cycle impact assessment results. This one-at-a-time approach sensitivity analysis does not assess the magnitude of the uncertainty of the final results, but is limited to information regarding the sensitivity of the model parameters, by indicating which parameters affect the final result most (Clavreul, Guyonnet, & Christensen, 2012; Groen, Heijungs, A. M. Bokkers, & Boer, 2014).

We make special note of the economic allocation used when modelling the solvent extraction process. Because the price of samarium is much lower than that of neodymium, the impacts of REO production are allocated mostly to neodymium. While in absolute terms less significant than the three parameters discussed above, we find that when changing the allocation of Sm_2O_3 from 0.5 % to 1% then the total GWP results increases 26%. But for Nd_2O_3 , if the allocation coefficient changes from 34% to 34.5% then the total GWP results do not significantly change. This means

that if use of samarium would increase, and subsequently the price of samarium would increase, the environmental impacts of SmCo magnets would also increase significantly.

3.2 Uncertainty Analysis

Each specific parameter in the model has inherent uncertainty and/or variability. The uncertainty analysis explores the three most sensitive parameters, as identified in section 3.1: REE content, base metal content, nickel coating layer thickness. Standard deviation was based on upper bound and lower bound of values found in literature, augmented with expert judgment (as described in section 2.3 and Supporting Information, Tables S-5, S-6, and S-7).

The results of our 1,000 sample Monte Carlo simulation show that the investigated parameters in the NdFeB are slightly more robust than for SmCo. However, in terms of absolute values, they are quite similar. After performing the Monte Carlo analysis, the GWP results for SmCo will deviate by at most 48%. For NdFeB magnets, the GWP results will deviate by at most 42%. Heijungs (2010) demonstrates that the base case results are equal to that of the median distribution of the GHG emissions. For both NdFeB and SmCo the baseline results of GHG emissions are near the outside fiftieth percentile. The range of uncertainty for each magnet around the coating, REE and alloying content is illustrated in the box plot in Figure 3.

Figure 3. Boxplot of the Monte Carlo uncertainty results for SmCo (blue) and NdFeB (blue lines) magnets, projected GHG emissions for the functional unit. The mean of the output distribution is represented by the X and the median is represented by a solid line within the box. The reference case, or original result scenario (red line), is computed based on the mode of the distribution for each input parameter surveyed.

4. Discussion

The largest contributing process for NdFeB is electroplating, totaling a 65% contribution.

Electroplating is also a significant factor in the impact of SmCo. However, in absolute terms, cobalt production is responsible for the largest fraction, 47% (Figure 1). Cobalt is an essential factor for SmCo products used in EV motor applications as it increases its thermal properties.

Our results imply that from an environmental point of view, it would be of interest to explore the

possibility of $\text{Sm}_2\text{Co}_{17}$ magnets as an alternative for NdFeB, since they generally contain about (50% by mass) less cobalt than SmCo.

At both room and higher temperatures, a SmCo magnet will outlast a NdFeB magnet (even when the latter is appropriately doped with dysprosium or terbium). Thus, if one would change the functional unit of this LCA to reflect multiple operation cycles, then one could see a relative reduction in the environmental impact of SmCo over NdFeB. However, since SmCo magnets from electric motors are not reused for multiple vehicle life cycles, this not likely to occur.

While there are no individually completed LCA studies to compare the impact assessment results of SmCo magnets, Nordelöf et al. (2019) updated Ecoinvent 3 data for SmCo and reworked with more accurate energy use data and a new economic allocation procedure. However, Nordelof et al (2019) chose to use the Ecoinvent cobalt dataset instead of the newer one from CDI which according to the LCA summary report from CDI could lead to about a 30% reduction in GWP results (Cobalt Development Institute, 2016).

When comparing the environmental profiles of samarium metal in Lee and Wen (2017) with this study, we see that Lee and Wen (2017) calculate for 1 kg of samarium metal around 106 kg of CO_2 equivalent is produced, whereas for we find 62 kg of CO_2 . Regarding the impacts related to NdFeB magnets, the kg of CO_2 equivalent values range from 89 kg to 41 kg in two recent publications, although direct comparability is difficult due to differing deposits, methodologies, and system boundaries (Arshi, Vahidi, & Zhao, 2018; Marx et al., 2018). These differences illustrates how REE life cycle data is still very much incomplete, particularly regarding the upstream processes (Bailey et al, 2020).

5. Conclusion

This study represents the first LCA effort on the production of SmCo magnets. The results are discussed in the context of substituting NdFeB with SmCo for electric vehicle (EV) applications.

We find that SmCo does not yeild an environmental improvement over NdFeB, with SmCo causing 135 kg of CO₂ emissions, compared to 30.2 kg for a functionally equivalent amount of NdFeB. Impacts other than CO₂ generally also favor NdFeB, albeit less so. Although these results only hold for the particular combination of data and assumptions used in this study, the magnitude of the difference is significant enough that we are confident of our conclusions. We note that due to economic allocation, and the fact that samarium oxide is much cheaper than neodymium oxide (9 euro/kg and 48 euro/kg, respectively), the relative environmental impact will change, but not the conclusion of this study. If use of samarium would increase, and subsequently the price of samarium would increase, the environmental impacts of SmCo magnets would also increase significantly.

Although the environmental impacts are not necessarily reduced, supply risk could be helped by diversifying the use of different REE materials such as samarium for magnets for EV motors. Switching from neodymium to samarium would therefore somewhat reduce exposure to REE criticality, although large-scale substitution might cause samarium to become the ‘new’ bottleneck in the REE balance, rather than neodymium and dysprosium (Binnemans & Jones, 2015). However, substitution of REEs with cobalt will not necessarily reduce criticality related issues, as the cobalt supply chain is also problematic on several fronts, including market concentration and labor issues (van den brink 2020).

While SmCo is not better environmentally, it helps reduce REE criticality by creating a larger pool of diverse supply for REE magnets which can provide a venue for supply chain resilience (Sprecher et al., 2015).

Results of this LCA study can be combined with future studies to contribute to the broad industrial aim of building the environmental profile of REEs for various applications. This, in turn, will lead to a better understanding of the environmental impacts of REE-containing products, including those in the electric mobility sector.

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